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2D Electrical Resistivity Tomography survey optimisation of solute transport in porous media

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Key words: Resistivity, Tomography, Porous media, ERT, 2D models.

The purpose of this study is to quantify experimentally the evolution of dissolved species in porous media from 2D resistivity models. Transport experiments are done at the lab level by performing flow in a model porous medium obtained by filling a transparent container with mono disperse glass beads. A tracer made by mixing a dissolved blue dye and a known NaCl concentration is injected with a constant flow rate through the porous medium already saturated by a transparent fluid. ERT measurements are acquired during the fluids flow. The measurement conditions and the inversion parameters are estimated so that the relation between spatial and temporal resolutions is optimised. A video follow-up is also carried out during the flow. A comparison of the temporal evolution of the NaCl concentration distribution estimated from ERT models with video analysis shows remarkable agreement.

Electrical resistivity tomography is used to detect the contaminant's plumes in saturated porous media using the resistivity contrasts between the fluids saturating initially the pore spaces and the moving fluids (Binley, 1996; Oldenborger *et al.*, 2007). Archie's law (1942) relates the measured bulk apparent conductivities to the fluids resistivity in the poral network via *a priori* information about the porosity and the particles cementation state. As previously shown by (Slater *et al.*, 2000), it is possible to use this method to estimate the tracer spatial repartition in terms of concentrations. This method is non-invasive and non-destructive, but it is based

on indirect measurements of the electrical properties. The electrical conductivity distribution is obtained through data inversion. However the non-unicity of solution can lead to misinterpretations of the geological reality. We test the model's reliability in laboratory conditions by experiments in porous media at mesoscopic level where the hydrodynamic parameters can be easily estimated. We optimise the protocols of measurements and inversions according to the medium's geometry for tracer follow-up. The built models are then expressed in terms of tracer concentration distribution on several time steps and compared to the estimated concentrations by a parallel video follow-up.

EXPERIMENT PROTOCOL

The flow experiments are carried out in a transparent Plexiglas container (with a volume of $V = H \times L \times E = 233.75 \text{ cm}^3$) filled with glass beads of 166 microns diameter. Porosity is $\Phi = 0.365$, close to the theoretical value estimated by (Gondret, 1994): the porous medium may be considered homogeneous and isotropic. Hydrodynamic parameters are supposed constant, and the edge effects on the porosity are neglected since the pores diameter is small in comparison to the wall dimensions (Gondret, 1994). A permeable nylon fabric of 100 μm mesh covers the lower opening of the container. This part is in contact with a tank which contains the tracer,

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whereas three injectors in the sealed upper cover ensure a constant flow rate (Fig. 1a). Two lines of twenty one electrodes of 1.5 mm diameter, spaced every 1 cm are installed along the edges of the cell (Fig. 1b). The first and the last electrode of each line are located respectively at 3.5 cm of the lower and upper opening of the container. This kind of electrodes configuration reproduces the measurements conditions used in a borehole.

Four experimental conditions must be respected in order to optimise the ERT follow-up of tracer propagation (Slater *et al.*, 2000):

- 1/ all the pore space is saturated;
- 2/ the matrix conductivity is low in comparison to tracer conductivity;
- 3/ temporal variations of electric conductivity are only due to conductivity changes of interstitial fluids;
- 4/ electrical conductivity is linearly related to tracer concentration.

Prior to any experiments, the tank in contact with the lower opening is filled by a transparent fluid, which is pumped upwards by the injectors until total saturation of the medium. This fluid is produced by dissolution of a small

Figure 1a: Schematic of the experimental Plexiglas cell filled with spherical glass beads of 125 to 166 micron diameter. $H=27.5$ cm, $L=8.5$ cm, $E=1$ cm.

Figure 1b: Side view of the experimental device. $s=1$ cm, $a=3.5$ cm, $b=21$ cm.

amount of NaCl in degassed and demineralised water. The pumping rate (1.5 ml/min) is sufficiently low to obtain a perfect saturation of the medium. The tracer is obtained by dissolution of 0.1 g/L blue dye mixed with 1.0 g/L NaCl in demineralised water.

The two fluids are miscible, have the same viscosity and their different NaCl concentration creates a small density difference. During the experiments a mixing zone appeared between the two fluids: its characteristics depend upon the densities contrasts, pore size and flow rate.

The geometry evolution of this zone is observed, at the same time, by two independent techniques: the video follow-up which links transmitted light intensity through the cell measured on each pixel of the camera to the dye concentration, and the electrical measurements which reveal

the NaCl dispersion during transport. The experiments are reproduced at several constant flow rates with different NaCl concentrations between the two fluids and different density differences.

ELECTRICAL MEASUREMENT PROTOCOL OPTIMISATION

A sensitivity analysis (Furman *et al.*, 2007) is necessary to estimate the best series of quadripoles to describe the dispersion front on each time-step, while minimizing the acquisition time. First we did a set of experiments where the pumping was stopped when the tracer filled half of the porous medium. In these conditions gravity stabilizes the front and its position is fixed. We have tested several standard protocol measurements (Wenner-Schlumberger, gradient, dipole-dipole). The first results show that the measurements are strongly perturbed by the resistive edges of the plexiglas tank. In order to remove this effect, data have to be normalised (Daily *et al.*, 1995; Nimmer *et al.*, 2008) and the inversion parameters are optimised to produce reliable models of conductivity distribution. Archie's law and linear relationship between conductivity and concentration (Fig. 2) allows to relate the bulk conductivity of each model to NaCl concentration. Vertical variations of dye concentrations estimated by video (red curve) and NaCl estimated by ERT (black curve) are compared. For all experiments, the two concentration curves are shifted: the mean position of the NaCl mixing front appears to be in advance in comparison to the dye. This shift is probably due to dye trapping in dead end pore zones and adsorption on particle surfaces.

DYNAMIC MONITORING OF THE MIXING FRONT

Tests carried out for a static front position allow the efficiency of each measurement protocol to be evaluated in description on the fluids interface. We found that a transversal dipole-dipole configuration with 190 quadripoles is best adapted to the geometry of our medium. The temporal resolution is also optimised: each time step is performed in 5 minutes while 30 minutes were needed for the measurements in static conditions. Yet, the continuous tracer propagation causes a temporal shift between the first and the last measurements of each time step. This drawback is corrected assuming a linear conductivity variation with time. Data analyses and inversion parameters are similar as in the case of static fluids (Fig. 3), vertical variations of concentrations estimated by both methods present the same tendencies.

Figure 2: Vertical variations concentrations of NaCl (C/C_0) and dye obtained by ERT (black curve) and video analysis (red curve).

Thickness and mean front position on first time steps are similar (Fig. 3), but the tracer propagation creates a shift of the mean front position which increases upward during the experiment.

Figure 3 (see color plate): Dynamic tracer follow-up in terms of electrical resistivity distribution and comparison with relative concentrations estimated on each time step.

CONCLUSIONS

• Optimisation of the electrical measurements protocol provides an acceptable compromise between spatial and temporal resolutions.

• Dynamics monitoring gives a reliable estimation of position and thickness of the mixing front.

• The shift observed between video and ERT is caused by adsorption and dye trapping, which may be quantified by our method.

In the future, it will be necessary to check on the repetitiveness of the results with several density differences and flow rates. The system will also be complexed, while adding permeability heterogeneities and a 2D vertical fracture.

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